

Characterization of shear-stresses in an oscillating grid bioreactor using bioluminescent micro-organisms

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Introduction and context

Microalgae and photobioreactors

The promotion of transfers within a reactor is often the keystone of the enhancement of a chemical or biochemical process. In the case of microorganism cultures within a bioreactor, this transfers intensification should not be accompanied by a shear stress increase inducing mechanical stress on the micro-organisms that can lead to their lysis. For the culture of microalgae, heterogeneous group of photosynthetic microorganisms, several configurations and geometries of photobioreactors (PBR) are available, each one with its own advantages and disadvantages^{1,2,3}:

Oscillating grid turbulence and fractal grid designs

Our thesis aim is to **design a PBR stirred by an oscillating grid**, stirring system classically used in fluid mechanics experiments to generate nearly isotropic and shear-free turbulent flows. The turbulence generated by an oscillating grid system can be monitored by the oscillation and grid parameters. This kind of stirring system was mainly used to study stratified and interfacial flows and sediments and particles sedimentations^{4,5}. Each grid used have a **fractal geometry** and is constructed in an A/2Eccentric wheel iterative way from a base pattern. In our case, we $\omega = 2 \cdot \pi \cdot \nu$ considered cross, square or I-shaped patterns. Rod Fractal grids were used as fixed grids to generate downstream turbulence in water or wind tunnels⁶. Grid support bar According to the triple Reynolds decomposition, we present some results of the mean (top right), oscillatory (bottom left) and turbulent flows (bottom right) obtained by a **PIV** method for the central plan of each grid (depicted by the green $z_{\rm eq}$ line). We considered A = 50 mm, $\nu = 1$ Hz, $z_{\text{water}} = L_{\text{tank}} = 249 \text{ mm and } z_{\text{eq}} = L_{\text{tank}}/2$.

Open culture systems Culture medium circulation provided by paddle wheels. Systems sensitive to external conditions





Mixing provided by bubbling and

shear stress depends on bubble sizes

Open raceway pond Bubble column

Flat plate airlift

Tubular PBR

Culture medium circulation

provided by centrifugal pump

generating shear stress

Closed culture systems

Stirred tank PBR

High induced shear-stress

Good mixing properties

Culture stirred by

rotating mobiles

generating shear

stresses in their

vicinity

Poor mixing properties Low induced shear-stress

Classification of microalgae according to their shear stress sensitivity:².

Cyanobacteria

Green microalgae

Red microalgae Haptophyta

Dinoflagelates **Diatoms**

Shear stress sensitivity

Microalgae culture aims: CO₂ capture and absorption, production of interest products as lipids (which can be transformed into biodiesel), photosynthetic pigments, proteins, vitamins or carbohydrates used for therapeutic, food or cosmetic purposes^{1,3}.

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Bioluminescence emitted by *Pyrocystis fusiformis*

During a student project, we proposed to design experiments at the interface between fluid mechanics measurements and microalgae cultures: take advantage of the **bioluminescence** ability of a **phytoplankton** specie when it is mechanically stressed by a flow to identify the high shear-stress area within our oscillating grid stirred photobioreactor. We decided to use the **dinoflagellate** specie **Pyrocystis fusiformis** which is non-toxic unlike the dinoflagellate well known for bioluminescence kind of experiments. this The bioluminescence is due to the enzymatic oxidation of the luciferin by the luciferase when the cell membranes are deformed and their permeability is modified by the action of shear-stress. The light is emitted when the oxidation product

returns to its ground state. *Pyrocystis fusiformis* follows a **circadian cycle** with 12 hours of light and 12 hours of dark. The bioluminescence only occurs during the **dark phase**^{7,8}.





Schedule-dependent light emission and shear-stress estimation

We stimulated the phytoplanktons each hour by starting the oscillation of the grid during 1 minute from the second hour after the end of the light phase (the light emission optimum lies between 2 and 6 hours after the end of the light phase). Between each stimulation, the culture was left to rest. To evaluate a potential tiredness of the culture due to previous stimulations, the same protocol was applied but only 2 and 5 hours after the end of the light phase. For each stimulation, the light emission was recorded and the global mean pixel intensity of each frames was computed.



Section Reality of the sector

model⁷ involving a critical shear-stress value beyond which the light emission can occur, we linked the pixel intensity to the local shear-stress. On the right, we present a comparison between



Pixel intensity of a recorded image of bioluminescence during the oscillation of a grid

were recorded with a CMOS camera LaVision Imager M-lite 5M.

bioluminescence and PIV experiments for shear-stress maps at similar and comparable moments.





Project conclusions and perspectives

Our results show a clear dependence of the light emission intensity on the hours in the circadian cycle leading to challenging reproducibility and repeatability. In addition to this cyclic behaviour, the bioluminescence intensity depends on the previous stimulations too. These information lead us to conclude that only one measurement per day can be performed to estimate the shear-stress with an appropriate calibration. The model used to estimate the shear-stress does not consider this time and previous stimulations dependence. In addition, the model used was established with simple laminar flows while oscillating grid flows are turbulent. All that being mentioned, the feasibility of such bioluminescence experiments in a complex flow configuration and with for now a simple optical setup highlight the potential for the use of *Pyrocystis fusiformis* as local flow shear-stress indicators for experimental investigations at the crossroad between fluid dynamics and bioprocess engineering.

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